

PAPER ID: 4049

Roll No.

--	--	--	--	--	--	--	--	--	--

**B.TECH.****ODD SEMESTER EXAMINATION (2017-18)****HEAT & MASS TRANSFER****Time: 3 Hours****Total Marks: 100****Note: Be precise and scientific in writing.****SECTION – A****1. Attempt ALL questions in brief.****(2X10= 20)**

- What do you understand by overall heat transfer coefficient?
- What is the significance of heat transfer?
- Explain effectiveness and efficiency of fin.
- Explain the significance of heisler's charts.
- Define Gray body.
- Define Prandtl number.
- What is intensity of radiation?
- What is radiation shield?
- Define condensation and their types.
- How heat exchangers are classified?

**SECTION – B****2. Attempt any THREE parts of the following.****(10X3= 30)**

- A furnace wall is composed of 220 mm of fire brick, 150 mm of common brick, 50 mm of 85% magnesia and 3mm of steel plate on the outside. if the inside surface temperature is 1500°C and outside surface temperature is 90°C, estimate the temperature between layers and calculate the heat loss in  $\text{Kj/h-m}^2$ . Assume,  $k$  (for fire brick) =  $4\text{kJ/m-h. }^\circ\text{C}$ ,  $k$  (for common brick) =  $2.8\text{kJ/m-h. }^\circ\text{C}$ ,  $k$  (for 85% magnesia) =  $2.4\text{kJ/m-h. }^\circ\text{C}$ ,  $k$  (steel) =  $240\text{kJ/m-h. }^\circ\text{C}$ .
- Derive an expression of rectangular fin in case of heat dissipation from an infinite long fin. What are advantages and application of fins?
- Castor oil at 25°C flows at a velocity of 0.1 m/s past a flat plate, in a certain process. If the plate is 4.5 m long and is maintained at a Uniform temperature of 95°C, calculate the following using exact solution:
  - The hydrodynamic and thermal boundary layer thicknesses on one side of the plate,
  - The total drag force per unit width on one side of the plane,
  - The local heat transfer coefficient at the trailing edge, and the heat transfer rate
- Explain diffuse emitter and radiation shape factor.
- Define pool boiling and also explain regimes of pool boiling with the help of diagram.

**SECTION – C****3. Attempt any ONE part of the following.****(10X1= 10)**

- A carbon steel plate ( $K = 45 \text{ W/m}^\circ\text{K}$ ) 600 mm x 900mm x 25 mm is maintained at 310°C. Air at 15°C blows over the hot plate. If convection heat transfer coefficient is  $22 \text{ W/m}^2\text{C}$  and 250 W is lost from the plate surface by radiation, calculate the inside plate temperature.
- Derive a general heat conduction equation in case of cylindrical co-ordinate.

**4. Attempt any ONE part of the following. (10X1= 10)**

- a. Prove that for a body whose thermal resistance is zero, the temperature required for cooling or heating can be obtained from the relation  $(t-t_a)/(t_i-t_a) = \exp[-Bi F_a]$ , where the symbols have their usual meanings
- b. A large metal plate of thickness 5cm is initially at 460°C. It is suddenly exposed to fluid at 100°C with a convection coefficient of 142.5W/m<sup>2</sup>.K. Find the time needed for its mid plane to reach a temperature of 316°C and surface temperature at the same instant of time. Take  $k= 21.25\text{W/m K}$  and  $\alpha = 1.2 \times 10^{-5} \text{ m}^2/\text{sec}$ .

**5. Attempt any ONE part of the following. (10X1= 10)**

- a. Derive the equation for boundary layer thickness.
- b. A 350mm long glass plate is hung vertically in the air at 24°C while its temperature is maintained at 80°C. Calculate the boundary layer thickness at the trailing edge of the plate. If a similar plate is placed in a wind tunnel and air is blown over it at a velocity of 5 m/s, find the boundary layer thickness at its trailing edge. Also determine the average heat transfer coefficient, for natural and forced convection for the above mentioned data.

**6. Attempt any ONE part of the following. (10X1= 10)**

- a. A small convex object of area  $A_1$ , temperature  $T_1$  and emissivity  $\epsilon_1$  is enclosed within a large enclosure at temperature  $T_2$  and emissivity  $\epsilon_2$ . Derive an expression for the net heat exchange between the two objects.
- b. Consider two large parallel plates one at  $t_1=27^\circ\text{c}$  with emissivity  $\epsilon_1=0.8$  and other at  $227^\circ\text{c}$  with emissivity  $\epsilon_2=0.4$ . An aluminum radiation shield with an emissivity,  $\epsilon_s=0.05$  on both sides is placed between the plates. Calculate the percentage reduction in heat transfer rate between the two plates as a result of shield. Use  $\sigma=5.67 \times 10^{-8} \text{ W/m}^2\text{K}^4$ .

**7. Attempt any ONE part of the following. (10X1= 10)**

- a. In a counter- flow double pipe heat exchanger; water is heated from 25°C to 65°C by oil with a specific heat of 1.45KJ/Kg K and mass flow rate of 0.9 Kg/s. The oil is cooled from 230°C to 160°C. If the overall heat transfer coefficient is 42070W/m<sup>2</sup>°C, calculate the following
  - i. the rate of heat transfer
  - ii. the mass flow rate of water and
  - iii. the surface area of the heat exchanger
- b. Derive an expression for effectiveness by NTU method for parallel flow.