

Printed Pages: 6

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EME-504

(Following Paper ID and Roll No. to be filled in your  
Answer Book)

Paper ID :140524

Roll No.

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B.Tech.

(SEM. V) THEORY EXAM. 2015-16

HEAT &amp; MASS TRANSFER (EME-504)

[Time:3 hours]

[MaximumMarks:100]

## SECTION-A

Q.1 Attempt all parts. All part carry equal marks. Write  
answer of each part in short. (2x10=20)

- (a) How do thermal conductivities of gases and non-metals vary with temperature?
- (b) Derive the expression for logarithmic mean area for the hollow cylinder.
- (c) Discuss the physical significance of effectiveness.
- (d) What do you understand by lumped system, explain it with suitable example?
- (e) Thermal time constant and response of temperature measuring instrument.

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- (f) Explain one-seventh power law over a flat plate.
- (g) Write down the assumptions which are made for the analysis of heat flow through the fin.
- (h) Discuss the following.
  - (i) Nusselt number and its physical significance.
  - (ii) Grashoff's number and its physical significance.
- (i) Write short note on fouling or scaling.
- (j) A gray diffuse opaque surface ( $\alpha = 0.8$ ) is at  $100^\circ\text{C}$  and receives an radiation  $1000 \text{ W/m}^2$ . If the surface area is  $0.1 \text{ m}^2$ . Calculate:
  - (i) Radiosity of the surface.
  - (ii) Net radiation heat transfer rate from the surface.
  - (iii) Calculate above quantities if the surface is black.

#### SECTION-B

Note: Attempt any five questions from this section.

(10x5=50)

Q.2. What do you mean by modes of heat transfer? Describe its governing laws in detail. Also describe the case of combined heat transfer by required expression.

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- Q.3 What is thermometer well, describe it with neat sketch and prove that the temperature measured by a thermometer well is not a true temperature of fluid.
- Q.4 What do you mean by radiation shield? Derive the expression of net heat transfer rate for a system of two parallel plates separated by  $n$ -shields of emissivity's  $\epsilon_1, \epsilon_2, \epsilon_3, \dots, \epsilon_n$ .
- Q.5 Give the detail classification of heat exchanger. Write down the governing parameters for analysis of heat exchanger. Also explain the compact heat exchanger with neat sketch.
- Q.6 Explain the following in details.
- (i.) Intensity of radiation.
  - (ii.) Shape factor algebra, facts and properties.
- Q.7 Steam in the condenser of a power plant is to be condensed at a temperature of  $30^\circ\text{C}$  with cooling water from a nearby lake, which enters the tubes of the condenser at  $14^\circ\text{C}$  and leaves at  $22^\circ\text{C}$ . The surface area of the tubes is  $45\text{ m}^2$  and the overall heat transfer coefficient is  $2100\text{ W/m}^2\text{ }^\circ\text{C}$ . Determine the mass flow rate of the cooling water needed and the rate of condensation of the steam in the condenser. Heat of vaporization of water at  $30^\circ\text{C}$   $2431\text{ kJ/kg}$ . and  $C_p = 4184\text{ J/kg }^\circ\text{C}$ .

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- Q.8 Determine the coefficient of heat transfer by free convection and maximum current density for a nichrom wire 0.5 mm in diameter. The surface of the wire is maintained at 300 °C. The wire is exposed to still air at 20 °C and resistance per meter length of the wire is 6 Ω/m Use relation:  $Nu=1.18 (Gr Pr)^{1/8}$ .

Use properties of air at 160 °C-

$$K_f = 0.0361 \text{ W/m K}, \quad \nu = 30.35 \times 10^{-6} \text{ m}^2/\text{s}, \quad Pr = 0.687$$

- Q.9 Consider a diffuse circular disk of diameter  $D$  and area  $A_1$  and a plane-diffuse surfaces of area  $A_2 \ll A_1$ . The surfaces are parallel and  $A_2$  is located at a distance  $L$  from the center of  $A_1$ .

Obtain the following expression for the view factor

$$F_{ij} = \frac{D^2}{D^2 + L^2}$$

### SECTION-C

Attempt any two questions from this section. (15x2=30)

- Q.10 (a) Derive the general heat conduction equation in Cartesian co-ordinate for homogeneous and isotropic material.

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- (b) A wall is constructed of several layers. The first layer consists of bricks ( $k=0.66 \text{ W/m K}$ ), 25 cm thick, the second layer is 2.5 cm thick mortar ( $k=0.7 \text{ W/m K}$ ), the third layer 10 cm thick limestone ( $k=0.66 \text{ W/m K}$ ) and outer layer of 1.25 cm thick plaster ( $k=0.7 \text{ W/m K}$ ). The heat transfer coefficients on interior and exterior of the wall fluid layers are  $5.8 \text{ W/m}^2 \text{ K}$  and  $11.6 \text{ W/m}^2 \text{ K}$ , respectively. Find:
- (i) Overall heat transfer coefficient, (ii) Overall thermal resistance per  $\text{m}^2$ , (iii) Rate of heat transfer per  $\text{m}^2$ , if the interior of the room is at  $26^\circ \text{C}$  while outer air is at  $7^\circ \text{C}$ , (iv) Temperature at the junction between mortar and limestone.

Q.11 (a) Write down the name of some common types of fin with neat sketch. Also derive the expression for heat dissipation through rectangular fin which is infinitely long.

- (b) A Copper pipe carrying refrigerant at  $-20^\circ \text{C}$  is 10 mm in outer diameter and is exposed to ambient at  $25^\circ \text{C}$  with convective coefficient of  $50 \text{ W/m}^2 \text{ K}$ . It is proposed to apply the insulation of material having thermal conductivity of  $0.5 \text{ W/m K}$ . Determine the thickness beyond which the heat gain will be reduced. Calculate the heat losses for 2.5 mm, 7.5 mm, and 15 mm thick layer of insulation over 1 m length.

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Q.12 (a) Describe the boundary layer thickness and derive the expression for energy thickness.

(b) An iron sphere of diameter 5 cm is initially at a uniform temperature of 225 °C. It is suddenly exposed to an ambient at 25 °C with convection coefficient of 500 W/m<sup>2</sup>k.

(i) Calculate the centre temperature 2 minute after the start of exposure.

(ii) Calculate the temperature at the depth of 1 cm from the surface after 2 minute of exposure.

(iii) Calculate the energy removed from the sphere during this period. Take thermo-physical properties of iron plate:

$$k=60 \text{ W/mK}, \rho=7850\text{kg/m}^3, C=460 \text{ J/Kg}, \\ \alpha = 1.6 \times 10^{-5} \text{ m}^2/\text{s}$$

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